1. Introduction

SF6 has been used in circuit breakers to extinguish arc during operations and in zero current time. High transferring heat properties and appropriate insulation resistance have made sulfur hexafluoride to be used almost exclusively in gas power switches [1, 2]. However, researchers have got some issues to substitute the SF6 gas in circuit breakers. From the top of these arguments, the environment concern can be considered and also the better operations such as: reduction of effective heat and chamber corrosion, are as interest [3-5]. Sulfur hexafluoride has some other side effects and has been known as a greenhouse gas based on the high infrared attractions, long life time in environment and recombination with oxygen. In recent years, other fluids such as CO2, CF3I and N2 have been clarified in terms of heat conduction, electrical conductivity and even viscosity, accompanying the variation of pressure and heat [3]. Comparing to SF6, CO2 has got lower insulating power and it has been almost always known as a greenhouse gas, but however, the researchers have become to conclusion that the CO2 can be substitute with the SF6 gas, because of its higher dielectric property and electronegative characteristics [6-10]. The CF3I can hence be of interest to perform as a breaker insulator. Here are some explanations for this pretense in terms of comparing CF3I with SF6:

1. Dielectric power compared to SF6 gas is the same
2. Lower global warming potential
3. Higher molecular stability

In previous researches, the analyses of substitutionary gases have carried out only by the theoretical data. In this paper, a 3-dimensional simulation has been accomplished in order to study how accompany of varying and different gases can be forced on the arc impact, and also the regarding results from the gases characteristics analysis are used,
in addition. Studying arc in a 3-dimension simulation is one of the most complex issues in plasma physics. Most likely, arc phenomenon is simulating with finite element method (FEM), which in this paper the same method is being used in order to processing the arc impact from diverse gases. FEM settings in the whole process are as follows:

1. Defining circuit breaker geometry
2. Setting boundaries and initial conditions
3. Selecting equations and importing functions proper to arc process
4. Setting solvers and time steps of simulation under transient state
5. Running and solving the equations

To modeling the arc impact in 3-dimensions, all the system ruling equations and their solving algorithms must be executed properly. As a response to the latest argument, the simulations have been carried out based on the magneto-hydrodynamic (MHD) equations and the arc 3-dimensions solving algorithms are assumed as it is discussed in [18]. The method discussed in [18] is actually recorded the arc impact with high speed camera, and the results are taken into account with the simulations which guarantees the solvation method.

When analyzing a whole system in a limited territory is of a matter, there is no need to simulate the whole geometry structures all in together. Just the effective and influenced phenomena would be enough to take into accounts in the simulations. To do so, only the nozzle, chamber, contacts, and the inlet/outlet fluid pores are assumed in the simulations. As a result, the procedure execution time, and simulation size are reduced and also it’s a faster convergence product.

One of the basic items that have to be obtained in the simulations process is the fluids characteristics. Using hydrodynamic and electric characteristics of the fluids makes it easier to simulate the fluids impact on the arc [3]. The fluids that are discussed in this article are: CO₂, CF₃I, and N₂, which will be compared to each other individually and also to SF₆. Assuming all the above mentioned items, in this paper, the fluids action in contrast with high current arcs will be discussed which can complement the previous studies.

2. System Ruling Equations

The relation between the arc current, magnetic field, and plasma flow are shaped in the form of magneto-hydrodynamic equation which is in relation with k-ε turbulence model [11,14] in which k and ε are turbulence kinetic energy and loss ratio. The k-ε model has been applied most of the times for modeling the plasma arc [13-15, 17-20]. In addition to k-ε model, other parameters like arc current distribution in 3-dimensions and self-magnetic field have to be calculated as well. The solution to arc current distribution can be expressed along the ohms’ law and can be calculated from the continuity equation \((\nabla \cdot \mathbf{j} = 0)\). The self-magnetic field can be derived from the ohms’ law by applying the magnetic potential field calculation.

The time related equations are described via mass conservation law, momentum conservation law, mass transferring via energy conservation law, and momentum and plasma flow energy.

Radiation is one of the important phenomena which can make the energy transferring system possible in arc plasma system [21]. The radiation linkage flux in a specific situation is a function of local properties, pressure and temperature. The absolute conductivity coefficient is used in most of the studies in order to calculate the arc phenomenon radiation [22], which is a validate result, so this method is nominated to simulate the radiation linkage flux.

A standard k-ε model is used to simulate the turbulence effect which is produced by arc and fluid. Variable parameters k and ε are related up to their own equations.

In analyzing the fluids, the heat transferring ability is in process to choose a suitable substitute from the heat transferring equations. Nevertheless, knowing that convection plays the key rule in heat transferring, Newton’s law of cooling is considered as follows:

\[
q = hA(T_w - T_f)
\]

where A is the connection surface area, \(T_w - T_f\) states the temperature difference between the fluid and the heat source, and h is the convective heat transferring coefficient. Normally, Newton’s law of cooling states that the rate of heat loss of a body is proportional to the difference in temperatures between the body and its surroundings. As such, it is equivalent to a statement that the heat transfer coefficient, which mediates between heat losses and temperature differences, is constant. From the given statement, it becomes obvious that the bigger surface area and higher temperature differences between the fluid and the heat source are, the more heat transfer is. In this paper the arc impact is well-defined and considered as the heat source. In addition, focusing on the other heat transferring impacts as describes below leads to an expert study:

1. Fluid physical properties: heat capacity, density, thermal conductivity coefficient, and viscosity in which the thermal conductivity coefficient is proportional to the heat conductivity.
2. Fluid motions
3. The geometry shape

All the mentioned factors influence the convective heat transferring coefficient. The fluid floating in breakers is a conclusion of the con-
tact movement and the piston below it, which is a compulsion reaction. In this paper, the fluid inlet velocity is assumed as 1 m/s. In the same condition, the convective compulsion coefficient is always bigger than the natural convective coefficient, which can differs more than 100 times. The Newton’s law of cooling says that \( h \) is not proportional to the temperature, but it is only true in compulsion convection coefficient under specific conditions, where in fact \( h \) is proportional to temperature difference \( (\Delta T) \) with a function to the power of 1/3 up to 1/4.

3. Simulations

In order to evaluate the operation quality of a fluid in circuit breaker for the mentioned fluids, a breaker with its structure characteristics has been chosen as a case study with voltage of 33 kV and 1250 A, where the simplified system is depicted in Fig. 1. The arc conductive parameters such as: electrical conductivity, specific heat capacity, dynamic viscosity, fluid density and thermal conductivity are proportional to pressure and temperature based on the gases individual properties. Transferring coefficients that are concluded from previous operational and theoretical studies \([3, 16]\) are used as assumption in the simulations. Based on the described equations on section 2, and also the magneto-hydrodynamic equations, all the calculations are fully considered in finite element method (FEM) \([17-20]\). There is also a notation of alternative arc current amplitude which is assumed up to 10000A (50 Hz) and also some initial conditions as follows:

Fluid initial temperature of 300K, and initial pressure of 0.35Mpa

The amount of temperature is known as an important value for the arc parameters and as an influence on physical properties. Temperature in different chamber areas has

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Fig. 1. The case study and fluid motion paths during the operation

Fig. 2. Thermal distribution between contacts in 5ms
also impacts on arc current distribution, arc resistance, and fluid physical properties (such as thermal conduction and viscosity). So, if the arc temperature can be reduced, it results on better breaker operation. Lower the arc temperature is, better the breaker operation is attached. The arc simulations for all mentioned fluids have been taken into the case study with the same condition respect. The main result of the fluid physical properties effect on their temperature during the first half period and thermal distribution in contacts region for different fluids is depicted in Fig. 2 (in 5ms). Maximum amplitude of current occurs in 5ms and temperature at this time is highest almost always. This process can create an option in which the different fluids can be compared during the maximum temperature in arc time. In Fig. 2, maximum temperature occurs respectively in \( CF_3I \), \( N_2 \), \( CO_2 \) and \( SF_6 \) eventually. Considering the lowest temperature that shows up in \( SF_6 \), it seems as if this fluid can operate better than the others. This is mainly because of the higher thermal conductivity of \( SF_6 \) in lower temperatures, and suitable molecular mass and higher specific heat capacity in temperatures between 15000K up to 30000K. Each specific fluid, reaches its maximum thermal conductivity in a known temperature valley. Considering the conductivity amount in reference [3], \( CF_3I \) in the temperature valley of 2000K up to 3000K has higher thermal conductivity than \( CO_2 \) and \( N_2 \). \( CO_2 \) and \( N_2 \) have higher thermal conductivity than \( CF_3I \) in the temperature range of 6000K up to 10000K. Highest thermal conductivity refers to \( SF_6 \) in temperature range of 1000K up to 2500K.

In temperatures more than 16000K, the highest thermal conductivity refers to \( SF_6 \) again. Higher thermal conductivity in lower temperatures is the cause of diffusion and thermal energy transferring, so, it brings decentralization in strict limits (as it is shown in Fig. 2. The thermal distribution in contacts region for is higher than the other fluids, and larger amount of the fluid concerns in the heat transferring process.)

Based on the higher molecular mass which is refers to \( CF_3I \), it gets higher thermal conductivity in a reasonable temperature valley, and therefore it is expected to operate just like \( SF_6 \) when it becomes to meet the arc. However, \( CF_3I \) in temperature ranges bigger than 15000K has lower thermal capacity and as a result its temperature gets higher with lower amounts of energy. In the mentioned temperature valley, \( CO_2 \) and \( N_2 \) have reasonable thermal capacity, but their lower molecular mass decreases the heat transferring a little bit.

Varying viscosity during the operation causes a limitation in fluid motion transferring at the arc boundary. Lower viscosity increases the fluid cooling ability and decreases the arc temperature during interrupting process. The viscosity of \( CF_3I \), \( N_2 \) and \( CO_2 \) is lower than \( SF_6 \) which is one of the benefits of the 3 mentioned fluids. The fluids highest viscosity happens in temperature valley from 7000K up to 15000K. In temperature valleys of 300K up to 7000K and 17000K up to 30000K, \( CF_3I \) and \( SF_6 \) viscosity almost coincides on scheme which means the viscosity amounts of these two fluids are so close, but in temperature valley of 7000K up to 17000K, \( CF_3I \) gets lower position than \( SF_6 \) on the scheme and it is expected to have a better cooling impact than \( SF_6 \). However, this differential issue is not enough to recompense the lower heat capacity of the \( CF_3I \) (In Fig. 3 the viscosity of the two fluids \( CF_3I \) and \( SF_6 \) are shown).

The \( CF_3I \) viscosity is lower in amounts which coincides the previous discussion. The average viscosity in the selected region for \( CF_3I \) is 1e-4 and for \( SF_6 \) is 1e-5. In the case of the two other fluids, this point is a little different, and their viscosity compared to \( SF_6 \), have a noticeable dissimilarity, therefore they have improved cooling condition. Especially \( CO_2 \) which is the lowest viscosity, threats in a similar manner as \( SF_6 \).

This argument can be fully discussed when maximum temperatures in arc channel are considered for different operation times (arc channel usually occurs between two contacts), therefore the fluids maximum temperature variations are curved in Fig. 4.
The result is similar to the previous conclusions where the lowest amount in maximum temperature for different operation times refers to $SF_6$ and $CO_2$ is the second ideal fluid in this study. The fluids cooling impact can be operated in many ways. Maximum temperature occurs in one spot or in a very limited region, so it cannot demonstrate the cooling power process alone. Therefore, the average temperature between the contacts in arc region is curved in Fig. 5 for all the mentioned fluids in half period. The results show the better operation of $CO_2$ and $SF_6$ all over again.

Temperatures rising between the contacts take place when the arc meets the fluid directly and causes the heat convection through the whole process. Considering the fact that the nozzle is located near the arc, there is no wonder if the warmed up fluid makes it evaporate. The best fluid operation occurs when the most heat, transfers through the edges in a time duration close to current peak, and hence, average fluid temperature during the arc in nozzle region must be brief to leads into lower evaporation. Temperature distribution analysis in nozzle region and current peak time is depicted in Fig. 6. It seems $CF_3I$ has the lowest amount in terms of heat transferring. In temperatures between 5000K up to 10000K, $CO_2$ and $N_2$ have higher thermal conductivity which show better operation in this
manner. CO₂ and N₂ have higher heat capacity than CF₃I and they pass through the nozzle with higher temperature that proves higher heat energy transferring by them. In general, it is true to say which fluid decreases arc channel temperature more has a better heat transferring and it is more succeeded to control the electric arc. Therefore, in this section, temperature rising in nozzle region is evaluated positively because it shows higher heat transferring through the arc edges in a limited space.

After analyzing heat transferring in the nozzle edges, probability and amount of the nozzle evaporation must be considered. To do this, average temperature of the nozzle region in Fig. 6 is achieved and an average temperature is calculated for the whole process. Table 1 shows the average temperature of the nozzle region through the arc impact (10ms) for all the under study fluids. According to Table 1, it is pointing higher average temperatures for CO₂ and N₂, which shows higher heat transferring through the arc edges as it was discussed earlier (this is one of the reason that reduces temperature in arc region). However, higher evaporation, nozzle corrosion, and life reduction are known as the side effects.

3.1. Arc Configuration in Zero Current Time

Controlling arc and extinguishing it in zero current time is the main reason to be used fluids in circuit breakers. Electrical conductivity has a non-linear proportion relation with temperature. In most temperature valleys, temperature rising causes electric conduction to be increased and arc resistance to be decreased. The operation is more succeeded if the arc channel temperature falls in zero current time. To compare fluids and their effects on distributed current between the contacts, current density near the zero current time is depicted in Fig. 7.

Current density has been curved for 1.2e5 A/m² and even lower amounts. Current has been turned off in the case of SF₆ and there are still some current surfaces in the case of the other 3 fluids. As current density domain increases, turn-off domain can be calculated. The object poses an amount which there is no higher current density exist between the contacts. The same trend is applied for the other 3 fluids, in which the current turn-off density for CF₃I is 7e5, for CO₂ is 3e5, and eventually for N₂ is 4e5.

### Table 1. Average temperature through the whole process in nozzle region

<table>
<thead>
<tr>
<th>Fluid</th>
<th>Average Temperature (K)</th>
</tr>
</thead>
<tbody>
<tr>
<td>SF₆</td>
<td>3661</td>
</tr>
<tr>
<td>CF₃I</td>
<td>4240</td>
</tr>
<tr>
<td>CO₂</td>
<td>4693</td>
</tr>
<tr>
<td>N₂</td>
<td>5063</td>
</tr>
</tbody>
</table>

![Fig. 6. Thermal distribution in the region close to the nozzle in maximum current (5ms)](image-url)
4. Conclusions

In order to substitute $SF_6$ gas in power circuit breakers, 3 basic fluids were analyzed in this paper. Then fluid characteristics were simulated in finite element method (FEM), and the results were taken out and compared from main point of view which is the temperature diffusion and current interruption time.

The average and maximum temperatures in arc region for $CO_2$ are close to the amount of $SF_6$ (in comparison to $N_2$ and $CF_3I$) and incidentally temperature distribution in $CO_2$ case is in a way that does not allow the temperature around the selected region for an nozzle like $N_2$ gets high. From the current turn-off view in moments close to the zero current, the maximum current density in $CO_2$ is lower than $N_2$ and $CF_3I$. According to the fluids characteristics and their operations during the arc, it seems that $CO_2$ has all the potential for the substitution. However, its recovery problem must be solved after zero current time, and also $CO_2$ molecular mass must be increased in order to increase the cooling power. To solve the latest issue, it can be recombined with heavier fluids. The two other fluids are not exempted from the very norm and their characteristics have to be modified for the use of high current electrical arc controlling. However, it seems as if they have better operation in the lower currents.

References


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